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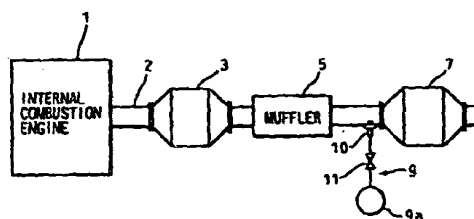
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### (54) A method for purifying combustion exhaust gas

(57) The method for purifying combustion exhaust gas according to the present invention utilizes a  $\text{NH}_3$  decomposing catalyst. The  $\text{NH}_3$  decomposing catalyst in the present invention is capable of converting substantially all of the  $\text{NH}_3$  in the combustion exhaust gas to  $\text{N}_2$  when the air-fuel ratio of the exhaust gas is lean and the temperature of the catalyst is within a predetermined optimum temperature range. Further, when the exhaust gas contains  $\text{NO}_x$  in addition to  $\text{NH}_3$ , the  $\text{NH}_3$  decomposing catalyst is capable of reducing the  $\text{NO}_x$  in the optimum temperature range even though the air-fuel ratio of the exhaust gas is lean. In the present invention, the conditions of the exhaust gas containing  $\text{NO}_x$  are adjusted before it is fed to the  $\text{NH}_3$  decomposing catalyst in such a manner that the temperature of the exhaust gas is within the optimum temperature range and the air-fuel ratio of the exhaust gas is lean. Further,  $\text{NH}_3$  is added to the exhaust gas before it is fed to the  $\text{NH}_3$  decomposing catalyst. Therefore, a lean air-fuel ratio exhaust gas, at a temperature within the optimum temperature range, which contains both the  $\text{NO}_x$  and  $\text{NH}_3$  is fed to the  $\text{NH}_3$  decomposing catalyst, and the  $\text{NO}_x$ , as well as the  $\text{NH}_3$ , in the exhaust gas is completely resolved by the  $\text{NH}_3$  decomposing catalyst.

Fig.1



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However, one problem arises when the process in the '917 publication is used for resolving HC, CO and NO<sub>x</sub> components. The three-way reducing and oxidizing catalyst, though it has a high ability for reducing NO<sub>x</sub> components in a reducing atmosphere, also converts a portion of NO<sub>x</sub> components in the exhaust gas to NH<sub>3</sub> component (ammonia) in a reducing atmosphere. In the process in the '917 publication, since the rich air-fuel ratio exhaust gas is fed to the three-way reducing and oxidizing catalyst, the exhaust gas flows out from the three-way reducing and oxidizing catalyst contains a small amount of NH<sub>3</sub>. This NH<sub>3</sub> in the exhaust gas is oxidized and again produces NO<sub>x</sub> when the exhaust gas is fed to the oxidizing catalyst in an oxidizing atmosphere. Therefore, when the process in the '917 publication is used, it is difficult to resolve NO<sub>x</sub> components in the exhaust gas completely, since NO<sub>x</sub> components are produced by the oxidizing catalyst.

## SUMMARY OF THE INVENTION

In view of the problems in the related art, the object of the present invention is to provide a process and a device for purifying a combustion exhaust gas which is capable of resolving substantially all of the HC, CO, and NO<sub>x</sub> components as well as a NH<sub>3</sub> component in the exhaust gas while preventing NO<sub>x</sub> from being produced by the oxidation of NH<sub>3</sub> contained in the exhaust gas.

The above object is achieved by a process for resolving an NH<sub>3</sub> component in a combustion exhaust gas by contacting a combustion exhaust gas containing an NH<sub>3</sub> component in an oxidizing atmosphere at a temperature within a predetermined range to an NH<sub>3</sub> decomposing catalyst which resolves the NH<sub>3</sub> component in an exhaust gas in an oxidizing atmosphere when the temperature of the catalyst is in the predetermined temperature range, converts the NH<sub>3</sub> component in the exhaust gas in an oxidizing atmosphere to NO<sub>x</sub> components when the temperature of the catalyst is high r than the predetermined temperature range, and allows the NH<sub>3</sub> component in the exhaust gas in an oxidizing atmosphere to pass through the catalyst when the temperature of the catalyst is lower than the predetermined temperature range.

The NH<sub>3</sub> decomposing catalyst is capable of resolving an NH<sub>3</sub> component in the exhaust gas in an oxidizing atmosphere when the temperature of the catalyst is within the predetermined temperature range. Therefore, by feeding the exhaust gas containing a NH<sub>3</sub> component to the NH<sub>3</sub> decomposing catalyst in an oxidizing atmosphere and at a temperature within the predetermined range, substantially all of the NH<sub>3</sub> component in the exhaust gas is resolved by the NH<sub>3</sub> decomposing catalyst without forming NO<sub>x</sub> components.

According to another aspect of the present invention, there is provided a process for resolving pollutants in the exhaust gas of an internal combustion engine comprising, contacting an exhaust gas of an internal combustion engine in a reducing atmosphere with an NH<sub>3</sub> synthesizing catalyst which converts NO<sub>x</sub> components in the exhaust gas, in a reducing atmosphere, to an NH<sub>3</sub> component, adjusting the conditions of the exhaust gas after it contacts the NH<sub>3</sub> synthesizing catalyst so that the exhaust gas is in an oxidising atmosphere and within a predetermined temperature range, and contacting the exhaust gas, after its atmosphere and temperature are adjusted, with an NH<sub>3</sub> decomposing catalyst which resolves an NH<sub>3</sub> component in the exhaust gas in an oxidizing atmosphere when the temperature of the catalyst is in a predetermined temperature range, converts the NH<sub>3</sub> component in the exhaust gas in an oxidizing atmosphere to NO<sub>x</sub> components when the temperature of the catalyst is higher than the predetermined temperature range, and allows the NH<sub>3</sub> component in the exhaust gas in an oxidizing atmosphere to pass through the catalyst when the temperature of the catalyst is lower than the predetermined temperature range.

In this aspect of the invention, the exhaust gas from the internal combustion engine contacts the NH<sub>3</sub> synthesizing catalyst in an reducing atmosphere. Therefore, the NO<sub>x</sub> component in the exhaust gas is converted to the NH<sub>3</sub> component. Further, after it contacts the NH<sub>3</sub> synthesizing catalyst, the exhaust gas contacts the NH<sub>3</sub> decomposing catalyst in an oxidizing atmosphere and at the temperature within the predetermined temperature range. Thus, substantially all of the NH<sub>3</sub> component produced by the NH<sub>3</sub> synthesizing catalyst is resolved by the NH<sub>3</sub> decomposing catalyst, and the exhaust gas flowing out from the NH<sub>3</sub> decomposing catalyst is completely free from the NO<sub>x</sub> and NH<sub>3</sub> components.

Further, the NH<sub>3</sub> synthesizing catalyst in the present invention is capable of resolving most of pollutants in the exhaust gas when the exhaust gas is in a reducing atmosphere (i.e., when the oxygen concentration in the exhaust gas is low). For example, the pollutants such as HC, CO and NO in the exhaust gas are resolved by the NH<sub>3</sub> synthesizing catalyst by the following reactions when the exhaust gas is in a reducing atmosphere.



and the  $\text{NH}_3$  component in the exhaust gas is effectively resolved by the  $\text{NH}_3$  decomposing catalyst even if the temperature of the exhaust gas at the outlet of the engine changes due to a change in the operating condition of the engine.

According to another aspect of the present invention, there is provided a process for resolving  $\text{NO}_x$  components in a combustion exhaust gas using an  $\text{NH}_3$  decomposing catalyst which resolves  $\text{NO}_x$  component in the exhaust gas in an oxidizing atmosphere under the presence of an  $\text{NH}_3$  component when the temperature of the catalyst is within a predetermined temperature range, converts the  $\text{NH}_3$  component in the exhaust gas in an oxidizing atmosphere when the temperature of the catalyst is higher than the predetermined temperature range, and allows the  $\text{NH}_3$  component in the exhaust gas in an oxidizing atmosphere to pass through the catalyst when the temperature of the catalyst is lower than the predetermined temperature range comprising, supplying  $\text{NH}_3$  to an exhaust gas from an internal combustion engine, and contacting the exhaust gas to the  $\text{NH}_3$  decomposing catalyst in an oxidizing atmosphere and at the temperature within the predetermined temperature range.

In this aspect of the invention, the  $\text{NH}_3$  decomposing catalyst resolves the  $\text{NO}_x$  components by reacting a  $\text{NH}_3$  component with  $\text{NO}_x$  components in the exhaust gas in an oxidizing atmosphere when the temperature is within a predetermined temperature range. Since  $\text{NH}_3$  is added to the exhaust gas before the exhaust gas is fed to the  $\text{NH}_3$  decomposing catalyst in this aspect of the invention, the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst in oxidizing atmosphere and at the temperature within the predetermined temperature range contains  $\text{NO}_x$  and  $\text{NH}_3$ , the  $\text{NO}_x$  components in the exhaust gas react with the  $\text{NH}_3$  component on the  $\text{NH}_3$  decomposing catalyst and are resolved.

According to another aspect of the present invention, there is provided a device for resolving  $\text{NO}_x$  components in the exhaust gas of an internal combustion engine operated at an air-fuel ratio higher than the stoichiometric air-fuel ratio comprising an  $\text{NH}_3$  decomposing catalyst disposed on an exhaust gas passage of an internal combustion engine, where in the  $\text{NH}_3$  decomposing catalyst resolves  $\text{NO}_x$  components in the exhaust gas flowing into the catalyst in an oxidizing atmosphere under the presence of an  $\text{NH}_3$  component when the temperature of the catalyst is in a predetermined temperature range, converts the  $\text{NH}_3$  component in the exhaust gas flowing into the catalyst in an oxidizing atmosphere to  $\text{NO}_x$  components when the temperature of the catalyst is higher than the predetermined temperature range, and allows the  $\text{NH}_3$  component in the exhaust gas in an oxidizing atmosphere to pass through the catalyst when the temperature of the catalyst is lower than the predetermined temperature range, an  $\text{NH}_3$  supply means for supplying  $\text{NH}_3$  to the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst, and temperature maintaining means for maintaining the temperature of the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst within the predetermined temperature range regardless of change in the temperature of the exhaust gas discharged from the internal combustion engine.

In this aspect of the invention, the internal combustion engine is operated at a lean air-fuel ratio and the exhaust gas from the engine is in an oxidizing atmosphere.  $\text{NH}_3$  is added to this exhaust gas before the exhaust gas flows into the  $\text{NH}_3$  decomposing catalyst. Further, the temperature of the exhaust gas is maintained within the predetermined range. Therefore, the exhaust gas containing  $\text{NO}_x$  components and a  $\text{NH}_3$  component is fed to the  $\text{NH}_3$  decomposing catalyst in an oxidizing atmosphere and at the temperature within the predetermined temperature range, and the  $\text{NO}_x$  components in the exhaust gas reacts the  $\text{NH}_3$  component at the  $\text{NH}_3$  decomposing catalyst and resolved.

According to another aspect of the present invention, there is provided a device for resolving  $\text{NO}_x$  components in an exhaust gas of an internal combustion engine operated at an air-fuel ratio higher than the stoichiometric air-fuel ratio comprising a plurality of  $\text{NH}_3$  decomposing catalysts disposed on the exhaust gas passage in series arrangement wherein each of the  $\text{NH}_3$  decomposing catalysts resolves  $\text{NO}_x$  components in the exhaust gas flowing into the catalyst in an oxidizing atmosphere under the presence of an  $\text{NH}_3$  component when the temperature of the catalyst is in a predetermined temperature range, converts the  $\text{NH}_3$  component in the exhaust gas flowing into the catalyst in an oxidizing atmosphere to  $\text{NO}_x$  components when the temperature of the catalyst is higher than the predetermined temperature range, and allows the  $\text{NH}_3$  component in the exhaust gas in an oxidizing atmosphere to pass through the catalyst when the temperature of the catalyst is lower than the predetermined temperature range, an  $\text{NH}_3$  supply means for supplying  $\text{NH}_3$  selectively to the exhaust gas flowing into the respective  $\text{NH}_3$  decomposing catalysts, temperature detecting means for detecting the temperature of the respective  $\text{NH}_3$  decomposing catalysts, and selecting means for controlling the  $\text{NH}_3$  supply means in such a manner that the  $\text{NH}_3$  supply means supplies  $\text{NH}_3$  to the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst(s) whose temperature is within the predetermined temperature range.

In this aspect of the invention, more than one  $\text{NH}_3$  decomposing catalysts are disposed on the exhaust gas passage of the engine. Since the temperature of the exhaust gas becomes lower as the exhaust gas flows down the exhaust gas passage, the temperatures of the respective  $\text{NH}_3$  decomposing catalysts vary in accordance with the location of the  $\text{NH}_3$  decomposing catalysts. Therefore, even when the temperature of the exhaust gas changes due to change in the operating condition of the engine, some of the  $\text{NH}_3$  decomposing catalysts always stay in the predetermined temperature range. A selecting means controls the  $\text{NH}_3$  supply means so that  $\text{NH}_3$  is supplied to the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalysts which has a temperature within the predetermined range. Therefore, exhaust gas in an oxidizing atmosphere containing  $\text{NH}_3$  and  $\text{NO}_x$  is fed to the  $\text{NH}_3$  decomposing catalyst which has the temperature within the predetermined range. Consequently, the  $\text{NO}_x$  component in the exhaust gas reacts the  $\text{NH}_3$  component at the  $\text{NH}_3$  decomposing catalyst and resolved.

In this aspect of the invention, the  $\text{NH}_3$  decomposing catalyst is also capable of absorbing the  $\text{NO}_x$  components in the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst when the engine operating air-fuel ratio is higher than the stoichiometric air-fuel ratio. Thus, the  $\text{NO}_x$  components are not discharged to atmosphere when the engine operating air-fuel ratio is higher than the stoichiometric air-fuel ratio. When the engine operating air-fuel ratio becomes lower than the stoichiometric air-fuel ratio, a  $\text{NH}_3$  component is produced by the  $\text{NH}_3$  synthesizing catalyst upstream of the  $\text{NH}_3$  decomposing catalyst. However, this  $\text{NH}_3$  component is oxidized at the  $\text{NH}_3$  decomposing catalyst by reacting the  $\text{NO}_x$  components absorbed by the  $\text{NH}_3$  decomposing catalyst. Therefore, both the  $\text{NO}_x$  and  $\text{NH}_3$  components are not discharged to atmosphere when the engine operating air-fuel ratio becomes lower than the stoichiometric air-fuel ratio.

## 10 BRIEF DESCRIPTION OF THE DRAWINGS

The present invention will be better understood from the description, as set forth hereinafter with reference to the accompanying drawings in which:

- 15 Fig. 1 is a drawing schematically illustrating an embodiment of the present invention when applied to an automobile engine;
- Fig. 2 is a drawing schematically illustrating another embodiment of the present invention;
- Fig. 3 is a drawing schematically illustrating another embodiment of the present invention;
- Fig. 4 is a drawing schematically illustrating another embodiment of the present invention;
- 20 Fig. 5 is a drawing schematically illustrating another embodiment of the present invention;
- Fig. 6 is a drawing showing the change in the characteristics of an  $\text{NH}_3$  decomposing catalyst in accordance with the change in the temperature; and
- Fig. 7 is a drawing schematically illustrating another embodiment of the present invention.

## 25 DESCRIPTION OF THE PREFERRED EMBODIMENT

In the embodiments explained hereinafter,  $\text{NH}_3$  decomposing catalysts are used for resolving  $\text{NO}_x$  and  $\text{NH}_3$  from a combustion exhaust gas. Therefore, an  $\text{NH}_3$  decomposing catalyst is explained before explaining the respective embodiments.

30 The  $\text{NH}_3$  decomposing catalyst in the embodiments of the present invention uses, for example, a honeycomb type substrate made of cordierite, and an alumina layer which act as a carrier for the catalyst is coated on the cell surface of the honeycomb substrate. On this carrier, at least one substance selected from elements belong to the fourth period or the eighth group in the periodic table of elements, such as copper (Cu), chrome (Cr), vanadium (V), titanium (Ti), iron (Fe), nickel (Ni), cobalt (Co), platinum (Pt), palladium (Pd), rhodium (Rh) and iridium (Ir) are carried as a catalyst.

35 The  $\text{NH}_3$  decomposing catalyst is capable of converting all the  $\text{NH}_3$  component in the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst to the  $\text{N}_2$  component provided that the exhaust gas is in an oxidizing atmosphere and the temperature of the catalyst is within a specific temperature range as determined by the substance being used as the catalyst. Therefore, when the exhaust gas is an oxidizing atmosphere containing a  $\text{NH}_3$  component and flows through the  $\text{NH}_3$  decomposing catalyst in this temperature range, the  $\text{NH}_3$  component in the exhaust gas is almost completely resolved, and the exhaust gas flows out from the  $\text{NH}_3$  decomposing catalyst contains no  $\text{NH}_3$  component. In the explanation below, this temperature range in which the  $\text{NH}_3$  decomposing catalyst can resolve all the  $\text{NH}_3$  component in the exhaust gas is called an optimum temperature range.

40 When the temperature of the  $\text{NH}_3$  decomposing catalyst is higher than the optimum temperature range, the  $\text{NH}_3$  component in the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst is oxidized by the  $\text{NH}_3$  decomposing catalyst and  $\text{NO}_x$  components are produced.

45 Namely, when the temperature of the  $\text{NH}_3$  decomposing catalyst is higher than the optimum temperature range, the oxidizing reaction of the  $\text{NH}_3$  component, i.e.,



50 become dominant on the  $\text{NH}_3$  decomposing catalyst, and the amount of  $\text{NO}_x$  components (mainly NO and  $\text{NO}_2$ ) in the exhaust gas flowing out from the  $\text{NH}_3$  decomposing catalyst increases.

Further, when the temperature of the  $\text{NH}_3$  decomposing catalyst is lower than the optimum temperature range, the oxidizing reaction of the  $\text{NH}_3$  component becomes lower, and the amount of the  $\text{NH}_3$  component in the exhaust gas flowing out from the  $\text{NH}_3$  decomposing catalyst increases.

55 Fig. 6 schematically illustrates the change in the characteristics of the  $\text{NH}_3$  decomposing catalyst in accordance with the change in the temperature. Fig. 6 shows the change in the concentration of the  $\text{NH}_3$  and  $\text{NO}_x$  components in the exhaust gas flowing out from the  $\text{NH}_3$  decomposing catalyst in accordance with the temperature of the  $\text{NH}_3$  decomposing catalyst when the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst is in an oxidizing atmosphere and the

$\text{NO}_x$  produced by the oxidizing reactions flows out from the  $\text{NH}_3$  decomposing catalyst without being reduced by the denitrating reactions.

On the other hand, when the temperature of  $\text{NH}_3$  decomposing catalyst is below the optimum temperature range, the oxidizing reactions hardly occur due to the low temperature. This causes the  $\text{NH}_3$  in the exhaust gas passes through the  $\text{NH}_3$  decomposing catalyst without being oxidized by the  $\text{NO}_x$  due to the shortage of the  $\text{NO}_x$  in the exhaust gas.

As explained above, the optimum temperature range of the  $\text{NH}_3$  decomposing catalyst is a temperature range in which the oxidizing reactions of the  $\text{NH}_3$  and the denitrating reactions of the  $\text{NO}_x$  balance each other in such a manner that the  $\text{NO}_x$  produced by the oxidation of the  $\text{NH}_3$  immediately reacts with  $\text{NH}_3$  in the exhaust gas without causing any surplus  $\text{NO}_x$  and  $\text{NH}_3$ . Consequently, the optimum temperature range of the  $\text{NH}_3$  decomposing catalyst is determined by the oxidizing ability of the catalyst and its temperature dependency. Therefore, when the catalyst component having high oxidizing ability, such as platinum (Pt), is used, the optimum temperature range becomes lower than that when the catalyst component having relatively low oxidizing ability, such as chrome (Cr) is used.

As explained above, though the mechanism of the phenomenon is not completely clarified, the  $\text{NH}_3$  decomposing catalyst actually converts all of the  $\text{NH}_3$  in the exhaust gas in an oxidizing atmosphere when the temperature is within the optimum temperature range. Further, when the  $\text{NH}_3$  decomposing catalyst is used in the optimum temperature range the following facts were found in connection with the above phenomenon:

(a) When the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst is in an oxidizing atmosphere, i.e., when the air-fuel ratio of the exhaust gas is lean compared to the stoichiometric air-fuel ratio, substantially all of the  $\text{NH}_3$  in the exhaust gas is converted to  $\text{N}_2$  without producing any  $\text{NO}_x$ . This occurs when the exhaust gas is in an oxidizing atmosphere (a lean air-fuel ratio), but regardless of the degree of leanness of air-fuel ratio of the exhaust gas. (In this specification, an air-fuel ratio of the exhaust gas at a certain point is defined by a ratio of the air and the fuel which are supplied to the combustion chambers or exhaust passages upstream of the point. Therefore, when no air or fuel is supplied in the exhaust passages upstream of the considered point, the air-fuel ratio of the exhaust gas at the point becomes the same as the air-fuel ratio of the air-fuel mixture supplied to the combustion chambers).

(b) When the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst contains  $\text{NO}_x$  in addition to  $\text{NH}_3$ , all of the  $\text{NO}_x$  in the exhaust gas as well as the  $\text{NH}_3$  is converted to  $\text{N}_2$ , and the concentration of the  $\text{NO}_x$  components in the exhaust gas becomes zero. In this case, the ratio of the concentrations of the  $\text{NO}_x$  components and the  $\text{NH}_3$  component is not necessarily stoichiometrical for the denitrating reactions (i.e., 4:3, or 1:1). It is only required that the exhaust gas contains an amount of  $\text{NH}_3$  more than the amount required for reducing the  $\text{NO}_x$  ( $\text{NO}_2$  and  $\text{NO}$ ) in the exhaust gas. As explained above, since the surplus  $\text{NH}_3$  in the exhaust gas is all converted to  $\text{N}_2$  when the exhaust gas is in an oxidizing atmosphere, no surplus  $\text{NH}_3$  is contained in the exhaust gas flowing out from the  $\text{NH}_3$  decomposing catalyst even in this case.

(c) When the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst contains HC and CO components, all of the HC and CO components are oxidized by the  $\text{NH}_3$  decomposing catalyst, provided that the air-fuel ratio of the exhaust gas is lean compared to the stoichiometric air-fuel ratio, and no HC and CO components are contained in the exhaust gas flowing out from the  $\text{NH}_3$  decomposing catalyst.

However, when the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst contains both the  $\text{NH}_3$  and  $\text{NO}_x$ , it was found that the temperature region IV in Fig. 6, i.e., the temperature region in which the concentration of  $\text{NO}_x$  components in the outflow exhaust gas increases as the temperature of the catalyst increases, moves to the lower temperature side compared to that when the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst contains only the  $\text{NH}_3$  components. This is because, when the exhaust gas contains  $\text{NO}_x$  in addition to  $\text{NH}_3$ , the  $\text{NO}_x$  in the inflow exhaust gas in addition to the  $\text{NO}_x$  produced by the oxidizing reaction of  $\text{NH}_3$  must be reduced by the  $\text{NH}_3$  in the exhaust gas. Consequently, the shortage of the  $\text{NH}_3$  is apt to occur in the relatively low temperature region. Therefore, when the exhaust gas contains both the  $\text{NH}_3$  and the  $\text{NO}_x$ , the optimum temperature range of the  $\text{NH}_3$  decomposing catalyst becomes narrower.

In relation to above (b), a conventional denitrating catalyst, such as a vanadia-titania ( $\text{V}_2\text{O}_5$ - $\text{TiO}_2$ ) type catalyst also has a capability for resolving  $\text{NH}_3$  and  $\text{NO}_x$  in the exhaust gas under a certain conditions. However, in case of the conventional denitrating catalyst, the amounts of  $\text{NH}_3$  and  $\text{NO}_x$  components must be strictly stoichiometrical in order to react  $\text{NH}_3$  with  $\text{NO}_x$  without causing any surplus  $\text{NH}_3$  and  $\text{NO}_x$ . Namely, when both the  $\text{NO}_2$  and  $\text{NO}$  are contained in the exhaust gas, the amount (moles) of the  $\text{NH}_3$  in the exhaust gas must be strictly equal to the total of the moles of  $\text{NO}_2$  in the exhaust gas multiplied by 3/4 and the moles of  $\text{NO}$  in the exhaust gas in order to react  $\text{NH}_3$  and  $\text{NO}_x$  without causing any surplus  $\text{NH}_3$  and  $\text{NO}_x$ . However, in case of the  $\text{NH}_3$  decomposing catalyst in the embodiments of the present invention, if the amount of the  $\text{NH}_3$  is more than the stoichiometrical compared to the amount of  $\text{NO}_x$ , and if the air-fuel ratio of the exhaust gas is lean, all of the  $\text{NH}_3$  and  $\text{NO}_x$  are converted to  $\text{N}_2$  without causing any surplus  $\text{NH}_3$  and  $\text{NO}_x$ . This is an important difference between the  $\text{NH}_3$  decomposing catalyst in the present invention and the conventional denitrating catalyst.

In this embodiment, the  $\text{NH}_3$  decomposing catalyst 7 is disposed on the exhaust gas passage downstream of the three-way reducing and oxidizing catalyst 3 in order to resolve the  $\text{NH}_3$  formed at the three-way reducing and oxidizing catalyst 3. Namely, the exhaust gas flows out from the three-way reducing and oxidizing catalyst 3 flows down the exhaust gas passage 2 and passes through the muffler 5. Further, air is added to the exhaust gas before it flows into the  $\text{NH}_3$  decomposing catalyst 7 by the secondary air supply unit 9.

Usually, the temperature of the exhaust gas at the outlet of the engine 1 is above the optimum temperature range of the  $\text{NH}_3$  decomposing catalyst 7. However, the temperature of the exhaust gas becomes lower as the exhaust gas flows down the exhaust gas passage due to the heat dissipation through the wall of the exhaust gas passage 2. Further, when it passes through the muffler 5, the exhaust gas is cooled by the muffler 5. Therefore, the temperature of the exhaust gas when it reaches the  $\text{NH}_3$  decomposing catalyst 7 is lower than the temperature at the outlet of the engine 1. In this embodiment, the length of the exhaust gas passage between the engine 1 and the  $\text{NH}_3$  decomposing catalyst 7 as well as the capacity of the muffler 5 is determined in such a manner that the temperature of the exhaust gas at the inlet of the  $\text{NH}_3$  decomposing catalyst 7 falls in the optimum temperature range even when the engine 1 is operated at the maximum exhaust temperature conditions. By this arrangement, the temperature of the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst 7, and the temperature of the  $\text{NH}_3$  decomposing catalyst 7 accordingly, is always maintained within the optimum temperature range regardless of the change in the operating conditions of the engine 1.

Further, the air-fuel ratio of the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst 7 is adjusted by supplying air from the secondary air supply unit 9 so that the air-fuel ratio of the exhaust gas becomes lean compared to the stoichiometric air-fuel ratio. As explained before, when the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst 7 is in an oxidizing atmosphere (i.e., at a lean air-fuel ratio), the  $\text{NH}_3$  decomposing catalyst 7 is capable of resolving substantially all of the  $\text{NH}_3$  in the exhaust gas regardless of the degree of the leanness of the air-fuel ratio of the exhaust gas. Therefore, it is not necessary to control the amount of air supplied from the secondary air supply unit 9 in order to strictly control the air-fuel ratio of the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst 7 in this embodiment. The amount of the air supplied from the secondary air supply unit 9 is set at an amount which can keep the air-fuel ratio of the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst 7 on a lean air-fuel ratio side compared to the stoichiometric air-fuel ratio even when the operating air-fuel ratio of the engine 1 fluctuates to the rich air-fuel ratio side compared to the stoichiometric air-fuel ratio.

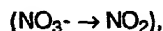
By the arrangement explained above, the exhaust gas supplied to the  $\text{NH}_3$  decomposing catalyst 7 is always an oxidizing atmosphere and has a temperature within the optimum temperature range. Therefore, even if  $\text{NH}_3$  is formed at the three-way reducing and oxidizing catalyst 3,  $\text{NH}_3$  is completely resolved by the  $\text{NH}_3$  decomposing catalyst 7. Further, when the air-fuel ratio of the exhaust gas becomes rich, the capability of the three-way reducing and oxidizing catalyst 3 for resolving HC and CO component in the exhaust gas decreases. However, according to the present embodiment, HC and CO components passing through the three-way reducing and oxidizing catalyst 3 are also resolved by the  $\text{NH}_3$  decomposing catalyst 7. Therefore, according to the present embodiment, an increase in the emission of HC, CO and  $\text{NH}_3$  components when the operating air-fuel ratio of the engine fluctuates to rich side can be prevented.

Though the temperature of the exhaust gas is adjusted by the heat dissipation from the wall of the exhaust gas passage 2 and the cooling by the muffler 5 in this embodiment, other means for adjusting the temperature of the exhaust gas may be used. For example, heat radiation fins may be disposed outer wall of the exhaust gas passage 2, instead of, or in addition to the muffler 5, or alternatively, the wall of the exhaust gas passage 2 may be water-cooled to increase the cooling capacity of the exhaust gas passage 2. Further, the amount of the air supplied from the secondary air supply unit 9 may be changed in accordance with the temperature of the exhaust gas to maintain the temperature of the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst 7 within the optimum temperature range by using a flow control valve instead of the shut off valve 11 in this embodiment. Further, the flow amount of the cooling water for cooling the exhaust gas passage wall, or the amount of the air supplied from the secondary air supply unit may be feedback controlled in accordance with an output signal of a temperature sensor detecting the catalyst bed of the  $\text{NH}_3$  decomposing catalyst 7 in such a manner that the temperature of the  $\text{NH}_3$  decomposing catalyst is maintained within the optimum temperature range.

In the above embodiment, if the operating air-fuel ratio of the engine 1 fluctuates to a lean air-fuel ratio side compared to the stoichiometric air-fuel ratio,  $\text{NH}_3$  is not formed at the three-way reducing and oxidizing catalyst 3, and the capability of the three-way reducing and oxidizing catalyst for reducing  $\text{NO}_x$  also decreases. In this case, an exhaust gas which contains  $\text{NO}_x$ , but does not contain  $\text{NH}_3$  flows into the  $\text{NH}_3$  decomposing catalyst 7. This causes the  $\text{NO}_x$  in the exhaust gas to pass through the  $\text{NH}_3$  decomposing catalyst 7 without being reduced. Therefore, to prevent the emission of the  $\text{NO}_x$  when the operating air-fuel ratio becomes lean, a  $\text{NO}_x$  absorbent which is capable of absorbing  $\text{NO}_x$  in the exhaust gas of a lean air-fuel ratio, or a  $\text{NO}_x$  reducing catalyst which has a capability for selectively reducing the  $\text{NO}_x$  in the exhaust gas even in an oxidizing atmosphere may be disposed on the exhaust gas passage 2 between the three-way reducing and oxidizing catalyst 3 and the  $\text{NH}_3$  decomposing catalyst 7. Fig. 7 shows an embodiment of the present invention in which a  $\text{NO}_x$  absorbent or a  $\text{NO}_x$  reducing catalyst is disposed on the exhaust gas passage 2 between the three-way reducing and oxidizing catalyst 3 and the  $\text{NH}_3$  decomposing catalyst 7. In Fig. 7, same reference

the form of nitric acid ions  $\text{NO}_3^-$ . Thus,  $\text{NO}_x$  in the exhaust gas is absorbed by the  $\text{NO}_x$  absorbent 8 when the air-fuel ratio of the exhaust gas is lean.

On the other hand, when the oxygen concentration in the exhaust gas becomes low, i.e., when the air-fuel ratio of the exhaust gas becomes rich, the production of  $\text{NO}_2$  on the surface of the platinum (Pt) is lowered and the reaction proceeds in an inverse direction



and thus nitric acid ions  $\text{NO}_3^-$  in the absorbent are released in the form of  $\text{NO}_2$  from the  $\text{NO}_x$  absorbent 8.

In this case, if the reducing substance such as  $\text{NH}_3$  and CO, or the substance such as HC and  $\text{CO}_2$  exist in the exhaust gas, the released  $\text{NO}_x$  is reduced on the platinum Pt by these components. Namely, the  $\text{NO}_x$  absorbent 8 performs the absorbing and releasing operation of the  $\text{NO}_x$  in the exhaust gas in which the  $\text{NO}_x$  in the exhaust gas is absorbed by the  $\text{NO}_x$  absorbent when the air-fuel ratio of the exhaust gas is lean and released from the  $\text{NO}_x$  absorbent when the air-fuel ratio of the exhaust gas becomes rich.

As explained in Fig. 6, the  $\text{NH}_3$  decomposing catalyst 7 converts the  $\text{NH}_3$  in the exhaust gas to  $\text{NO}_x$  when the temperature becomes higher than the optimum temperature range. Therefore, if the exhaust gas temperature at the outlet of the engine 1 becomes very high in an extreme operating condition of the engine 1, the temperature maintaining means such as the muffler 5 might be insufficient to lower the exhaust gas temperature to the optimum temperature range of the  $\text{NH}_3$  decomposing catalyst 7. In such a case, since the temperature of the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst 7 exceeds the optimum temperature range,  $\text{NO}_x$  is formed at the  $\text{NH}_3$  decomposing catalyst 7 and is discharged to atmosphere.

In this embodiment, the  $\text{NO}_x$  absorbent 8 is disposed on the exhaust gas passage 2 downstream of the  $\text{NH}_3$  decomposing catalyst 7 to prevent the emission of the  $\text{NO}_x$  in the extremely high exhaust gas temperature conditions. Since the  $\text{NO}_x$  absorbent 8 absorbs the  $\text{NO}_x$  in the exhaust gas in an oxidizing atmosphere, the  $\text{NO}_x$  formed at the  $\text{NH}_3$  decomposing catalyst 7 in the extremely high exhaust gas temperature condition is absorbed by the  $\text{NO}_x$  absorbent 8 and the emission of the  $\text{NO}_x$  to the atmosphere does not occur.

As explained above, according to the present embodiment, the exhaust emission can be always kept low even when the exhaust gas temperature becomes extremely high.

Though the  $\text{NO}_x$  absorbent 8 in the above embodiment is disposed on the exhaust gas passage 2 separately, it is possible to give the absorbing and releasing capability of  $\text{NO}_x$  to the substrate of the  $\text{NH}_3$  decomposing catalyst. This is accomplished by attaching the  $\text{NO}_x$  absorbing substances such as alkali metals and alkali-earth metals to the substrate of the  $\text{NH}_3$  decomposing catalyst 7 in addition to the catalytic components.

Next, another embodiment of the present invention is explained. In this embodiment, an  $\text{NO}_x$  reducing catalyst is disposed on the exhaust gas passage downstream of the  $\text{NH}_3$  decomposing catalyst 7 instead of the  $\text{NO}_x$  absorbent 8 in Fig. 2. Other constructions of this embodiment are the same as those in Fig. 2. Therefore, illustration of this embodiment by drawings is omitted.

The  $\text{NO}_x$  reducing catalyst in this embodiment has a substrate made of, for example, zeolite ZSM-5, and metals such as copper (Cu) and iron (Fe) are attached to the substrate by an ion exchange method. Alternatively, a substrate made of zeolite such as mordenite and precious metal such as platinum (Pt) attached thereon can also be used as the  $\text{NO}_x$  reducing catalyst. The  $\text{NO}_x$  reducing catalyst traps  $\text{NH}_3$ , HC and CO components in the exhaust gas in the pores of the porous zeolite, and selectively reduces the  $\text{NO}_x$  in the exhaust gas using these trapped components even in an oxidizing atmosphere.

In this embodiment, the  $\text{NO}_x$  reducing catalyst disposed at downstream of the  $\text{NH}_3$  decomposing catalyst 7 in Fig. 2 traps the  $\text{NH}_3$  component in the exhaust gas which passes through the  $\text{NH}_3$  decomposing catalyst 7 when the exhaust gas temperature is below the optimum temperature range as well as the HC and CO components in the exhaust gas. Further, when the exhaust gas temperature is above the optimum temperature range, the  $\text{NO}_x$  reducing catalyst selectively reduces the  $\text{NO}_x$  formed at the  $\text{NH}_3$  decomposing catalyst 7 using the trapped  $\text{NH}_3$ , HC and CO components. Therefore, according to the present embodiment, the  $\text{NO}_x$  formed at the  $\text{NH}_3$  decomposing catalyst in the high exhaust gas temperature conditions is not emitted to atmosphere and the exhaust emissions are always maintained at low level regardless of the change in the operating conditions of the engine.

Next another embodiment of the present invention is explained with reference to Fig. 3. In Fig. 3, the same reference numerals as those in Fig. 1 designate the same elements.

In this embodiment, means for cooling the exhaust gas such as the muffler 5 in Fig. 1 is not used. Further, a plurality of the  $\text{NH}_3$  decomposing catalyst are disposed on the exhaust gas passage 2 downstream of the three-way reducing and oxidizing catalyst 3 (Fig. 3 shows the case in which three  $\text{NH}_3$  decomposing catalyst 7a to 7c are used). Also, the secondary air supply unit 9 in this embodiment has a plurality of the nozzles 10a to 10c which are each disposed, in the exhaust gas passage 2, at the inlet of the respective  $\text{NH}_3$  decomposing catalysts 7a to 7c. Reference numeral 30 in Fig. 3 designates a control circuit of the engine 1. The control circuit 30 may be comprises, for example, a micro-computer of known type and performs basic controls of the engine 1 such as a fuel injection control and an ignition timing control.



posed on the exhaust gas passage 42. However, a three-way reducing and oxidizing catalyst 3 as shown in Fig. 5 is not provided in this embodiment. Further, instead of the secondary air supply unit 9 in Fig. 1, an  $\text{NH}_3$  supply unit 49 which comprises a nozzle 50 and a shut off valve 51 which are similar to those in Fig. 1 and a  $\text{NH}_3$  supply source 49a such as a bottle containing gaseous or liquid  $\text{NH}_3$  is provided in this embodiment.

In this embodiment, the exhaust gas in an oxidizing atmosphere from the lean burn engine 41 is cooled by the muffler 45 and flows into the  $\text{NH}_3$  decomposing catalyst 47 at the temperature within the optimum temperature range. Further,  $\text{NH}_3$  is added to the exhaust gas at the portion upstream of the  $\text{NH}_3$  decomposing catalyst 47. The exhaust gas from the lean burn engine 41 contains a relatively large amount of  $\text{NO}_x$ . Thus, the exhaust gas flowing into the  $\text{NH}_3$  decomposing catalyst is adjusted so that it becomes an oxidizing atmosphere and a temperature within the optimum temperature range. Further, the exhaust gas contains  $\text{NO}_x$  and  $\text{NH}_3$ . Therefore, both the  $\text{NO}_x$  and the  $\text{NH}_3$  in the exhaust gas are completely resolved by the  $\text{NH}_3$  decomposing catalyst 47.

As explained before, the capability of the three-way reducing and oxidizing catalyst for reducing the  $\text{NO}_x$  becomes very small when the exhaust gas is in an oxidizing atmosphere. Therefore, it is difficult to resolve the  $\text{NO}_x$  in the exhaust gas of the lean burn engine using the three-way reducing and oxidizing catalyst. However, according to the present invention, the  $\text{NO}_x$  in the exhaust gas from the lean burn engine can be completely resolved by the  $\text{NH}_3$  decomposing catalyst 47.

Further, the method for resolving  $\text{NO}_x$  in the exhaust gas of in an oxidizing atmosphere by adding an  $\text{NH}_3$  component to the exhaust gas and using a conventional vanadia-titania ( $\text{V}_2\text{O}_5\text{-TiO}_2$ ) type denitrating catalyst is known in the art. In the above conventional method,  $\text{NO}_x$  and  $\text{NH}_3$  are converted to  $\text{N}_2$  and  $\text{H}_2\text{O}$  by the denitrating reactions ( $8\text{NH}_3 + 6\text{NO}_2 \rightarrow 12\text{H}_2\text{O} + 7\text{N}_2$  and/or  $4\text{NH}_3 + 4\text{NO}_2 + \text{O}_2 \rightarrow 6\text{H}_2\text{O} + 4\text{N}_2$ ). However, in the conventional method, the amount of  $\text{NO}_x$  components and the  $\text{NH}_3$  component must be adjusted so that the ratio of the moles of  $\text{NO}_x$  and  $\text{NH}_3$  are strictly stoichiometrical (i.e., 4:3 or 1:1) in order to react  $\text{NO}_x$  with  $\text{NH}_3$  without causing any surplus  $\text{NO}_x$  and  $\text{NH}_3$ , as explained before.

However, in the actual operation of the engine, the concentration of the  $\text{NO}_x$  components in the exhaust gas varies widely in accordance with the operating condition of the engine, and it is difficult to control the amount of the  $\text{NH}_3$  added to the exhaust gas in accordance with the concentration of the  $\text{NO}_x$  in the exhaust gas. Therefore, if the conventional method is used for an actual engine,  $\text{NO}_x$  or  $\text{NH}_3$  is emitted to the atmosphere in some cases.

However, in case of the  $\text{NH}_3$  decomposing catalyst 47 in this embodiment, it is not required to strictly control the amount of the  $\text{NH}_3$  added to the exhaust gas since the  $\text{NH}_3$  decomposing catalyst can convert all of the  $\text{NH}_3$  in the exhaust gas as long as the exhaust gas is in an oxidizing atmosphere. In this embodiment, it is only required that the amount of the  $\text{NH}_3$  added to the exhaust gas is sufficiently large to reduce all of the  $\text{NO}_x$  in the exhaust gas while maintaining the exhaust gas in an oxidizing atmosphere. Therefore, according to the present embodiment, the  $\text{NO}_x$  in the exhaust gas of the lean burn engine can be completely resolved by a simple control of the  $\text{NH}_3$  supply unit 49 while preventing the emission of  $\text{NH}_3$ .

Fig. 5 shows another embodiment of the present invention which is similar to the embodiment in Fig. 3. In this embodiment, a plurality of the  $\text{NH}_3$  decomposing catalysts (47a to 47c in Fig. 5) and  $\text{NH}_3$  supply nozzles (50a to 50c in Fig. 5) are disposed on the exhaust gas passage 42. Similarly to the embodiment in Fig. 3, the control circuit 30 selects the  $\text{NH}_3$  decomposing catalyst which is in the optimum temperature range according to the operating conditions of the engine 41, and supplies  $\text{NH}_3$  to those  $\text{NH}_3$  decomposing catalysts through the  $\text{NH}_3$  nozzle located at the inlet of those  $\text{NH}_3$  decomposing catalysts. Since the operation of the present embodiment is substantially the same as the operation of the embodiment in Fig. 3, a detailed explanation is not given here.

From the description set forth above, it will be understood that, according to the present invention, the  $\text{NH}_3$  and  $\text{NO}_x$  components contained in the combustion exhaust gas can be resolved effectively by the  $\text{NH}_3$  decomposing catalyst. Though the present invention is explained using the embodiments in which the present invention is applied to the internal combustion engine, the application of the present invention is not limited to the internal combustion engine. The present invention can be also applied to resolve the  $\text{NH}_3$  and  $\text{NO}_x$  components in the exhaust gas discharged from the combustion devices other than the internal combustion engine. Namely, the present invention can be also applied to, for example, boilers, furnaces etc., which emit combustion exhaust gases.

The method for purifying combustion exhaust gas according to the present invention utilizes a  $\text{NH}_3$  decomposing catalyst. The  $\text{NH}_3$  decomposing catalyst in the present invention is capable of converting substantially all of the  $\text{NH}_3$  in the combustion exhaust gas to  $\text{N}_2$  when the air-fuel ratio of the exhaust gas is lean and the temperature of the catalyst is within a predetermined optimum temperature range. Further, when the exhaust gas contains  $\text{NO}_x$  in addition to  $\text{NH}_3$ , the  $\text{NH}_3$  decomposing catalyst is capable of reducing the  $\text{NO}_x$  in the optimum temperature range even though the air-fuel ratio of the exhaust gas is lean. In the present invention, the conditions of the exhaust gas containing  $\text{NO}_x$  are adjusted before it is fed to the  $\text{NH}_3$  decomposing catalyst in such a manner that the temperature of the exhaust gas is within the optimum temperature range and the air-fuel ratio of the exhaust gas is lean. Further,  $\text{NH}_3$  is added to the exhaust gas before it is fed to the  $\text{NH}_3$  decomposing catalyst. Therefore, a lean air-fuel ratio exhaust gas, at a temperature within the optimum temperature range, which contains both the  $\text{NO}_x$  and  $\text{NH}_3$  is fed to the  $\text{NH}_3$  decomposing catalyst, and the  $\text{NO}_x$ , as well as the  $\text{NH}_3$ , in the exhaust gas is completely resolved by the  $\text{NH}_3$  decomposing catalyst.



9. A device according to claim 7, further comprising an NO<sub>x</sub> reducing catalyst which selectively reduces NO<sub>x</sub> components in the exhaust gas in an oxidizing atmosphere and is disposed on the exhaust gas passage downstream of said NH<sub>3</sub> decomposing catalyst.

10. A device for resolving an NH<sub>3</sub> component contained in the exhaust gas of an internal combustion engine comprising:

a plurality of NH<sub>3</sub> decomposing catalysts disposed in an exhaust gas passage of an internal combustion engine in series arrangement, each of said NH<sub>3</sub> decomposing catalysts resolving an NH<sub>3</sub> component in the exhaust gas flowing into the catalyst in an oxidizing atmosphere when the temperature of the catalyst is in a predetermined temperature range, converts the NH<sub>3</sub> component in the exhaust gas flowing into the catalyst in an oxidizing atmosphere to NO<sub>x</sub> components when the temperature of the catalyst is higher than said predetermined temperature range, and allowing the NH<sub>3</sub> component in an exhaust gas in an oxidizing atmosphere to pass through the catalyst when the temperature of the catalyst is lower than said predetermined temperature range;

oxygen supply means for supplying oxygen selectively to the exhaust gas flowing into the respective NH<sub>3</sub> decomposing catalysts;

temperature detecting means for detecting the temperature of the respective NH<sub>3</sub> decomposing catalysts; and

selecting means for controlling said oxygen supply means in such a manner that the oxygen supply means supplies oxygen to the exhaust gas flowing into the NH<sub>3</sub> decomposing catalyst(s) whose temperature is within said predetermined temperature range.

11. A process for resolving NO<sub>x</sub> components from a combustion exhaust gas using an NH<sub>3</sub> decomposing catalyst which resolves NO<sub>x</sub> component in the exhaust gas in an oxidizing atmosphere under the presence of an NH<sub>3</sub> component when the temperature of the catalyst is within a predetermined temperature range, converts the NH<sub>3</sub> component in the exhaust gas in an oxidizing atmosphere to NO<sub>x</sub> components when the temperature of the catalyst is higher than said predetermined temperature range, and allows the NH<sub>3</sub> component in the exhaust gas in an oxidizing atmosphere to pass through the catalyst when the temperature of the catalyst is lower than said predetermined temperature range comprising:

supplying NH<sub>3</sub> to a combustion exhaust gas; and

contacting the exhaust gas with the NH<sub>3</sub> decomposing catalyst in an oxidizing atmosphere and at the temperature within said predetermined temperature range.

12. A device for resolving NO<sub>x</sub> components in the exhaust gas of an internal combustion engine operated at an air-fuel ratio higher than the stoichiometric air-fuel ratio comprising:

an NH<sub>3</sub> decomposing catalyst disposed on an exhaust gas passage of an internal combustion engine, said NH<sub>3</sub> decomposing catalyst resolves NO<sub>x</sub> components in the exhaust gas flowing into the catalyst in an oxidizing atmosphere under the presence of an NH<sub>3</sub> component when the temperature of the catalyst is in a predetermined temperature range, converts the NH<sub>3</sub> component in the exhaust gas flowing into the catalyst in an oxidizing atmosphere to NO<sub>x</sub> components when the temperature of the catalyst is higher than said predetermined temperature range, and allows the NH<sub>3</sub> component in the exhaust gas in an oxidizing atmosphere to pass through the catalyst when the temperature of the catalyst is lower than said predetermined temperature range;

NH<sub>3</sub> supply means for supplying NH<sub>3</sub> to the exhaust gas flowing into said NH<sub>3</sub> decomposing catalyst; and

temperature maintaining means for maintaining the temperature of the exhaust gas flowing into said NH<sub>3</sub> decomposing catalyst within said predetermined temperature range regardless of a change in the temperature of the exhaust gas discharged from the internal combustion engine.

13. A device for resolving NO<sub>x</sub> components in an exhaust gas of an internal combustion engine operated at an air-fuel ratio higher than the stoichiometric air-fuel ratio comprising:

a plurality of NH<sub>3</sub> decomposing catalysts disposed in the exhaust gas passage in series arrangement, each of said NH<sub>3</sub> decomposing catalysts resolving NO<sub>x</sub> components in the exhaust gas flowing into the catalyst in an oxidizing atmosphere under the presence of an NH<sub>3</sub> component when the temperature of the catalyst is in a predetermined temperature range, converts the NH<sub>3</sub> component in the exhaust gas flowing into the catalyst in an oxidizing atmosphere to NO<sub>x</sub> components when the temperature of the catalyst is higher than said predetermined temperature range, and allows the NH<sub>3</sub> component in the exhaust gas in an oxidizing atmosphere to pass through the catalyst when the temperature of the catalyst is lower than said predetermined temperature range;

NH<sub>3</sub> supply means for supplying NH<sub>3</sub> selectively to the exhaust gas flowing into the respective NH<sub>3</sub> decomposing catalysts;

temperature detecting means for detecting the temperature of the respective NH<sub>3</sub> decomposing catalysts;

and

21. A device according to claim 10, wherein said  $\text{NH}_3$  decomposing catalyst contains an  $\text{NH}_3$  adsorbing component which adsorbs an  $\text{NH}_3$  component in the exhaust gas.

22. A device according to claim 12, wherein said  $\text{NH}_3$  decomposing catalyst contains an  $\text{NH}_3$  adsorbing component which adsorbs an  $\text{NH}_3$  component in the exhaust gas.

23. A device according to claim 13, wherein said  $\text{NH}_3$  decomposing catalyst contains an  $\text{NH}_3$  adsorbing component which adsorbs an  $\text{NH}_3$  component in the exhaust gas.

24. A process according to claim 17, wherein said  $\text{NH}_3$  adsorbing component adsorbs an  $\text{NH}_3$  component in the exhaust gas when the temperature is lower than said predetermined temperature range.

25. A process according to claim 18, wherein said  $\text{NH}_3$  adsorbing component adsorbs an  $\text{NH}_3$  component in the exhaust gas when the temperature is lower than said predetermined temperature range.

26. A process according to claim 19, wherein said  $\text{NH}_3$  adsorbing component adsorbs an  $\text{NH}_3$  component in the exhaust gas when the temperature is lower than said predetermined temperature range.

27. A device according to claim 20, wherein said  $\text{NH}_3$  adsorbing component adsorbs an  $\text{NH}_3$  component in the exhaust gas when the temperature is lower than said predetermined temperature range.

28. A device according to claim 21, wherein said  $\text{NH}_3$  adsorbing component adsorbs an  $\text{NH}_3$  component in the exhaust gas when the temperature is lower than said predetermined temperature range.

29. A device according to claim 22, wherein said  $\text{NH}_3$  adsorbing component adsorbs an  $\text{NH}_3$  component in the exhaust gas when the temperature is lower than said predetermined temperature range.

30. A device according to claim 23, wherein said  $\text{NH}_3$  adsorbing component adsorbs an  $\text{NH}_3$  component in the exhaust gas when the temperature is lower than said predetermined temperature range.

31. A device according to claim 20, wherein said  $\text{NH}_3$  adsorbing component comprises an acidic inorganic substance.

32. A device according to claim 21, wherein said  $\text{NH}_3$  adsorbing component comprises an acidic inorganic substance.

33. A device according to claim 22, wherein said  $\text{NH}_3$  adsorbing component comprises an acidic inorganic substance.

34. A device according to claim 23, wherein said  $\text{NH}_3$  adsorbing component comprises an acidic inorganic substance.

35. A device according to claim 20, wherein said  $\text{NH}_3$  adsorbing component comprises at least one substance selected from zeolite, silica ( $\text{SiO}_2$ ), titania ( $\text{TiO}_2$ ), silica-alumina ( $\text{SiO}_2\text{-Al}_2\text{O}_3$ ) copper (Cu), cobalt (Co), nickel (Ni) and iron (Fe).

36. A device according to claim 21, wherein said  $\text{NH}_3$  adsorbing component comprises at least one substance selected from zeolite, silica ( $\text{SiO}_2$ ), titania ( $\text{TiO}_2$ ), silica-alumina ( $\text{SiO}_2\text{-Al}_2\text{O}_3$ ) copper (Cu), cobalt (Co), nickel (Ni) and iron (Fe).

37. A device according to claim 22, wherein said  $\text{NH}_3$  adsorbing component comprises at least one substance selected from zeolite, silica ( $\text{SiO}_2$ ), titania ( $\text{TiO}_2$ ), silica-alumina ( $\text{SiO}_2\text{-Al}_2\text{O}_3$ ) copper (Cu), cobalt (Co), nickel (Ni) and iron (Fe).

38. A device according to claim 23, wherein said  $\text{NH}_3$  adsorbing component comprises at least one substance selected from zeolite, silica ( $\text{SiO}_2$ ), titania ( $\text{TiO}_2$ ), silica-alumina ( $\text{SiO}_2\text{-Al}_2\text{O}_3$ ) copper (Cu), cobalt (Co), nickel (Ni) and iron (Fe).

Fig. 2

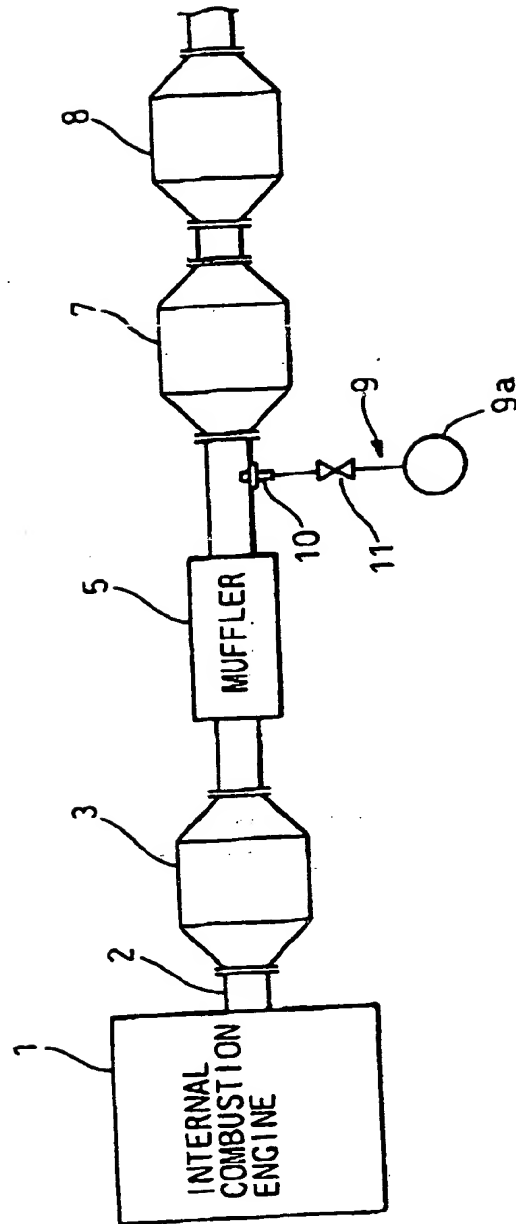


Fig. 4

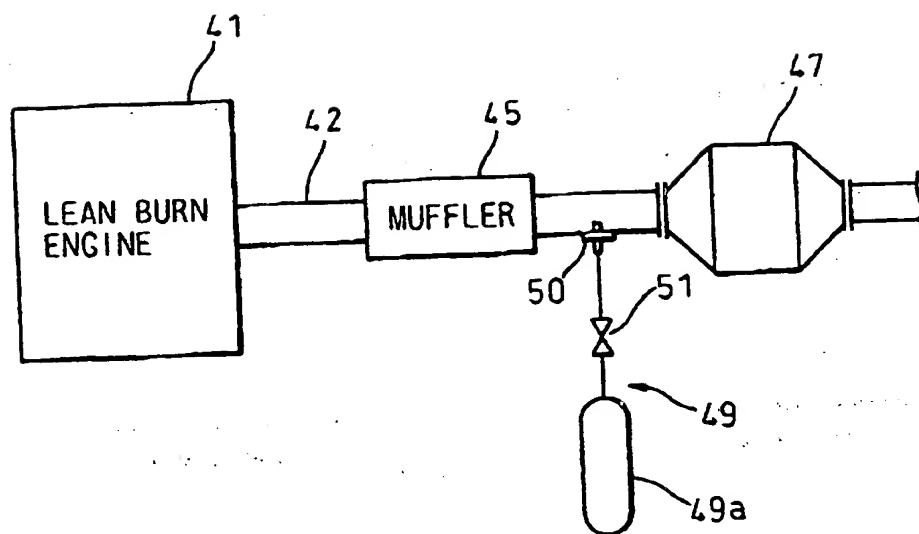
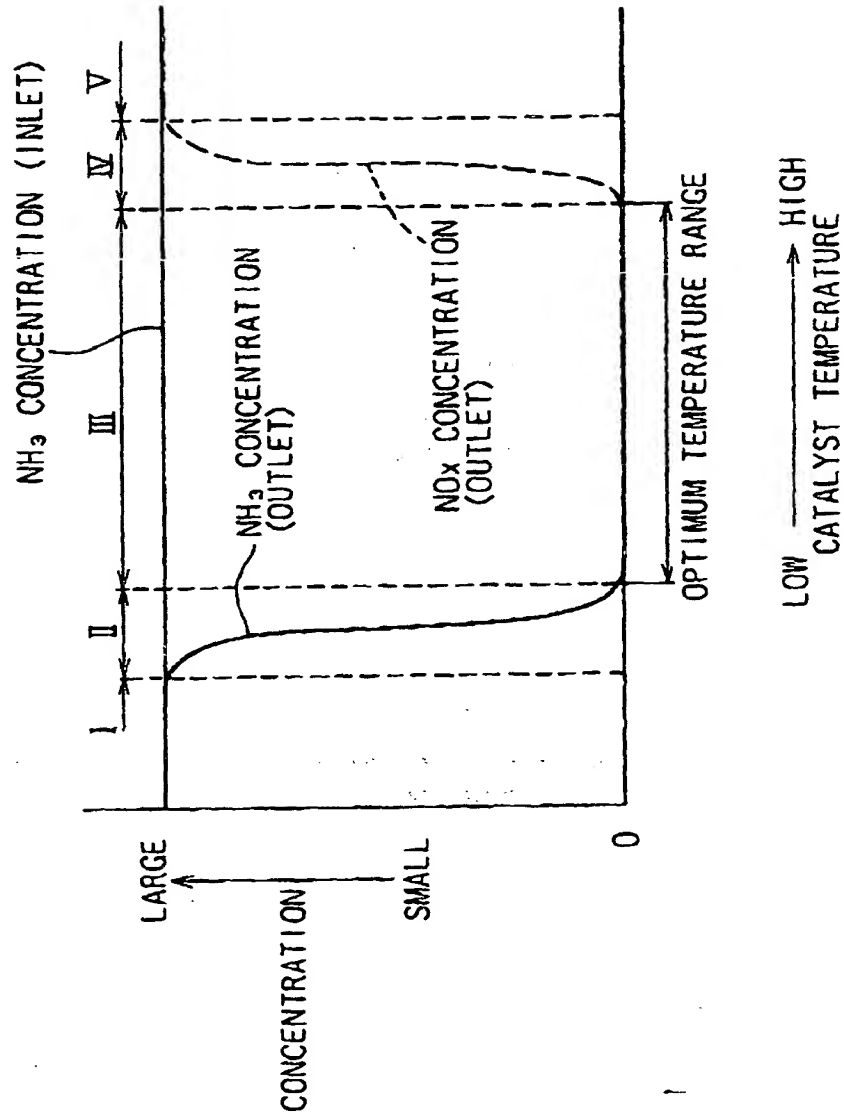
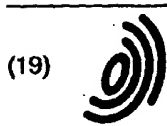


Fig. 6





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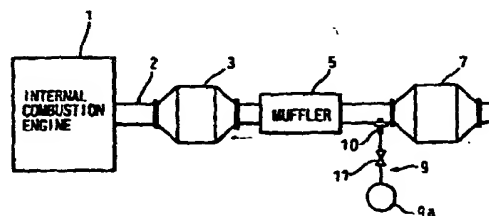
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### (54) A method for purifying combustion exhaust gas

(57) The method for purifying combustion exhaust gas according to the present invention utilizes a  $\text{NH}_3$  decomposing catalyst. The  $\text{NH}_3$  decomposing catalyst in the present invention is capable of converting substantially all of the  $\text{NH}_3$  in the combustion exhaust gas to  $\text{N}_2$  when the air-fuel ratio of the exhaust gas is lean and the temperature of the catalyst is within a predetermined optimum temperature range. Further, when the exhaust gas contains  $\text{NO}_x$  in addition to  $\text{NH}_3$ , the  $\text{NH}_3$  decomposing catalyst is capable of reducing the  $\text{NO}_x$  in the optimum temperature range even though the air-fuel ratio of the exhaust gas is lean. In the present invention, the conditions of the exhaust gas containing  $\text{NO}_x$  are adjusted before it is fed to the  $\text{NH}_3$  decomposing catalyst in such a manner that the temperature of the exhaust gas is within the optimum temperature range and the air-fuel ratio of the exhaust gas is lean. Further,  $\text{NH}_3$  is added to the exhaust gas before it is fed to the  $\text{NH}_3$  decomposing catalyst. Therefore, a lean air-fuel ratio exhaust gas, at a temperature within the optimum temperature range, which contains both the  $\text{NO}_x$  and  $\text{NH}_3$  is fed to the  $\text{NH}_3$  decomposing catalyst, and the

$\text{NO}_x$ , as well as the  $\text{NH}_3$ , in the exhaust gas is completely resolved by the  $\text{NH}_3$  decomposing catalyst.

Fig. 1



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